Calculation in our website is based on the following formula.
This calculation is a simple calculation that does not include valve data.
■ Non-Choked Flow ( $\Delta p<0.5 p_{1}$ )

|  | CV Value | Flow Rate | Differential Pressure (Pressure Loss) |
| :---: | :---: | :---: | :---: |
| Liquid | $\mathrm{C}_{\mathrm{V}}=11.6 Q \sqrt{\frac{G_{f}}{\Delta p}}$ | $Q=\frac{\mathrm{C}_{\mathrm{V}}}{11.6} \sqrt{\frac{\Delta p}{G_{f}}}$ | $\Delta p=\left(\frac{11.6 Q}{C_{V}}\right)^{2} \cdot G_{f}$ |
| Gas | $\mathrm{C}_{\mathrm{V}}=\frac{V}{2.78} \sqrt{\frac{G_{g} T_{1}}{\Delta p\left(p_{1}+p_{2}\right)}}$ | $V=2.78 C_{V} \sqrt{\frac{\Delta p\left(p_{1}+p_{2}\right)}{G_{g} T_{1}}}$ | $\Delta p=p_{1}-\sqrt{p_{1}{ }^{2}-\left(\frac{V}{2.78 \times C_{V}}\right)^{2} \times G_{g} T_{1}}$ |
| Saturation <br> Steam | $\mathrm{C}_{\mathrm{V}}=\frac{7260 W}{\sqrt{\Delta p\left(p_{1}+p_{2}\right)}}$ | $W=\frac{C_{V}}{7260} \sqrt{\Delta p\left(p_{1}+p_{2}\right)}$ | $\Delta p=p_{1}-\sqrt{p_{1}{ }^{2}-\left(\frac{7260 W}{C_{V}}\right)^{2}}$ |
| Superheated <br> Steam | $\mathrm{C}_{\mathrm{V}}=\frac{7260 W\left(1+0.0013 T_{S H}\right)}{\sqrt{\Delta p\left(p_{1}+p_{2}\right)}}$ | $W=\frac{C_{V}}{7260\left(1+0.0013 T_{S H}\right)} \sqrt{\Delta p\left(p_{1}+p_{2}\right)}$ | $\Delta p=p_{1}-\sqrt{p_{1}{ }^{2}-\left(\frac{7260 W\left(1+0.0013 T_{S H}\right)}{C_{V}}\right.}$ |

Choked Flow ( $\Delta p \geqq 0.5 p 1$ )

|  | Cv Value | Flow Rate | Differential Pressure (Pressure Loss) |
| :---: | :---: | :---: | :---: |
| Liquid | Not Applicable | Not Applicable |  |
| Gas | $\mathrm{C}_{\mathrm{V}}=\frac{V}{2.43} \frac{\sqrt{G_{g} T_{1}}}{p_{1}}$ | $V=2.43 \mathrm{C}_{\mathrm{V}} \frac{p_{1}}{\sqrt{G_{g} T_{1}}}$ | Not Applicable |
| Saturation <br> Steam | $\mathrm{C}_{\mathrm{V}}=\frac{8340 W}{p_{1}}$ | $W=\frac{\mathrm{C}_{\mathrm{V}}}{8340} \cdot p_{1}$ | Not Applicable |
| Superheated <br> Steam | $\mathrm{C}_{\mathrm{V}}=\frac{8340 W\left(1+0.0013 T_{S H}\right)}{p_{1}}$ | $W=\frac{\mathrm{C}_{\mathrm{V}}}{8340\left(1+0.0013 T_{S H}\right)} \cdot p_{1}$ | Not Applicable |

Explanation of Symbols

| $C v$ | Flow Coefficient (Cv Value) |
| :---: | :--- |
| $V$ | Gas Volume Flow Rate $\left(\mathrm{Nm}^{3} / \mathrm{h}\right)$ |
| $p_{1}$ | Absolute Static Pressure Upstream of Valve (kPa abs) <br> $\Delta p$ |
| Differential Pressure between Upstream and <br> Downstream Valve (kPa) $(\Delta p=p 1-p 2)$ |  |
| $G g$ | Specific Gravity of Gas at Standard Condition <br> compared to Air at Standard Condition |
|  | As air being one (1). |
| $T 1$ | Absolute Temperature Upstream of valve (K) |
| $T S H$ | Degree of Superheat $\left({ }^{\circ} \mathrm{C}\right)$ |

$Q \quad$ Liquid Volume Flow Rate ( $\mathrm{m}^{3} / \mathrm{h}$ )
$W$ Mass Flow Rate ( $\mathrm{t} / \mathrm{h}$ )
$p 2$ Absolute Static Pressure Downstream of Valve (kPa abs)
Gf Specific Gravity of Liquid at Operating Temperature compared to Water at Standard Condition As water being one (1).
$T 1$ Absolute Temperature Upstream of valve (K)
T SH Degree of Superheat ( ${ }^{\circ} \mathrm{C}$ )
Even if the differential pressure (differential pressure between upstream and downstream of the valve) is increased, in choked flow condition flow rate does not increase.


Figure 1: Relationship between Differential Pressure and Flow Rate

